





Agenda

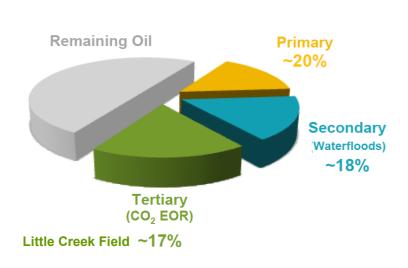
- Introduction to EOR Processes
- Design Steps of CO₂ EOR
- Mechanism Important to Process
- Advances in Hybrid EOR Processes
- Practical Workflow & Case Studies
- Conclusions

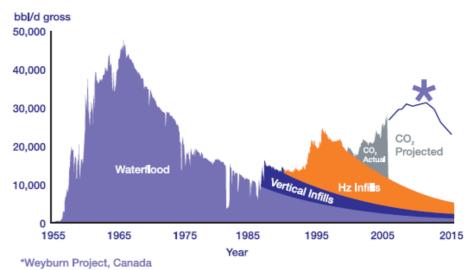




Why EOR Processes?

Oil recoveries from primary and secondary recovery phases are generally in the range of 20–40% of OOIP



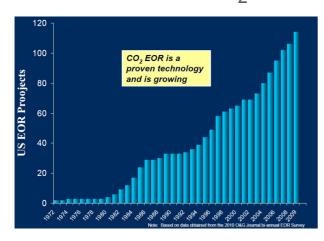




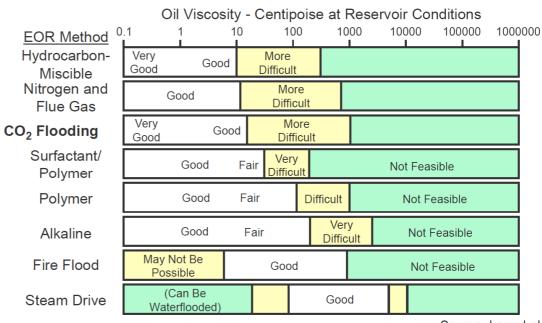
Why CO₂ EOR?

Two major advantages:

- Additional oil recovery
- CO₂ storage to reduce emissions of CO₂



@ 2012 Chevron



Source: Larry Lake



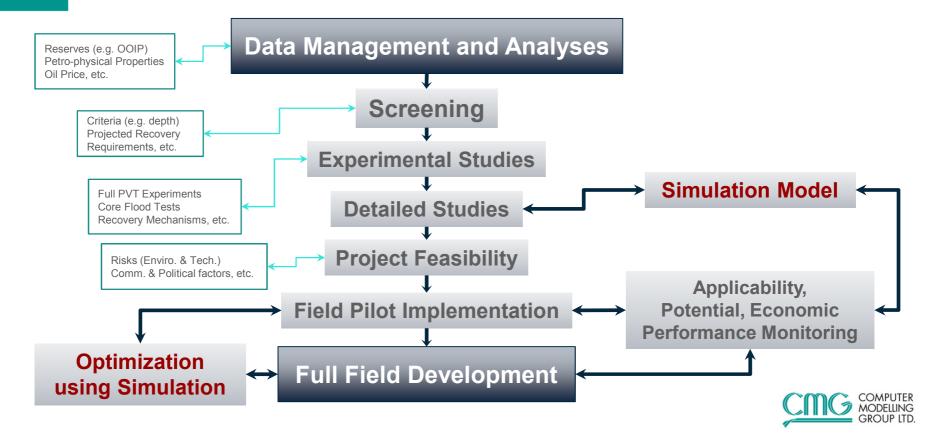


Miscible or Immiscible CO₂ EOR?

- Proven to be technically feasible in miscible and immiscible modes
- Among 123 CO₂-EOR projects in the United States, 114 are miscible projects (koottungal, 2012; kuuskraa, 2012)
- Mainly on light to ultra-light oils (>28°API) with a viscosity of less than 3 centipoise



Design Steps of CO₂ EOR



What Does Reservoir Modelling Aim at?

Better Understanding of Reservoir Performance





Steps to Make a Representative Model?

STEP 1: Reliable data Input

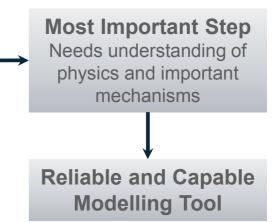
Reservoir Parameters, PVT, etc.

STEP 2: History Matching

Production and pressure history data

STEP 3: Forecast

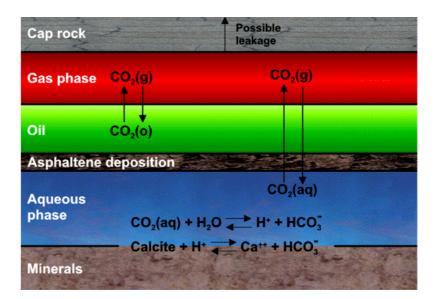
Different scenarios, optimum design, etc.





CO₂ EOR Mechanisms

- PVT, solubility, and swelling
- Miscibility mechanisms
- Asphaltene deposition
- Wettability Alteration
- Hysteresis
- IFT Effects
- Diffusion and Dispersion





Additional Process Mechanisms

- Matrix dissolution from CO₂ injection
- Aqueous chemical equilibrium reactions
- Ion-exchange
- Mineralization: dissolution and precipitation
- Thermal effects
- CO₂ leakage through caprock





What to Use?



Advanced general equation-of-state compositional simulator

Simulates compositional effects of reservoir fluid during primary and enhanced oil recovery processes



Phase behaviour and reservoir fluid property program for PVT modelling and data matching

For modelling of:

- Gas condensates
- Tight/shale gas
- CO₂ EOR
- WAG
- Chemical EOR
- CO₂ Sequestration
- LSW flooding
- Polymer Flooding
- ASP flooding
- •





What to Use?





Sensitivity Analysis

- Better understanding of a simulation model
- Identify important parameters



History Matching

- · Calibrate simulation model with field data
- Obtain multiple history-matched models



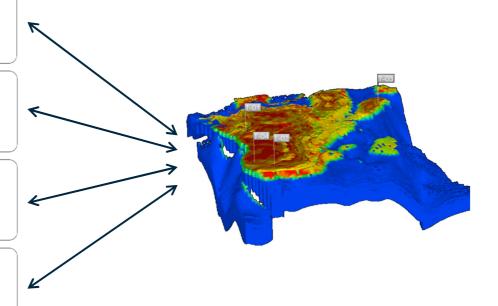
Optimization

- Improve NPV, Recovery, ...
- Reduce cost



Uncertainty Analysis

- Quantify uncertainty
- Understand and reduce risk

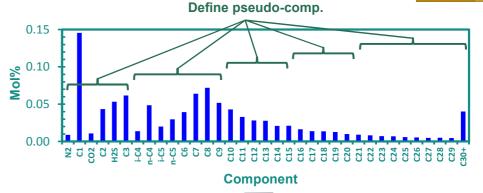


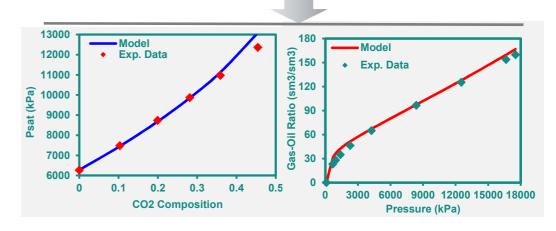






- Fluid Characterization
 - Compositional Analysis
 - Recombination
- Lab Data Matching
 - \rightarrow *P*, *T*, and composition variation
 - CCE
 - Differential liberation
 - Separator test
 - Swelling test



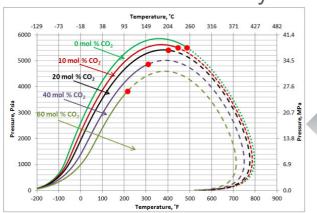


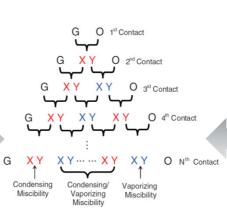


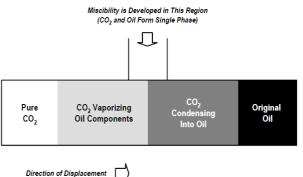
Miscibility Mechanisms

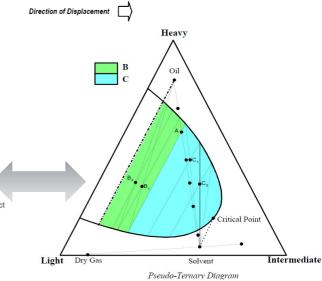


- · Vaporizing, condensing, combined
- MMP and MME determination
- Methods
 - Cell to Cell
 - Multiple Mixing Cell
 - Semi-Analytical









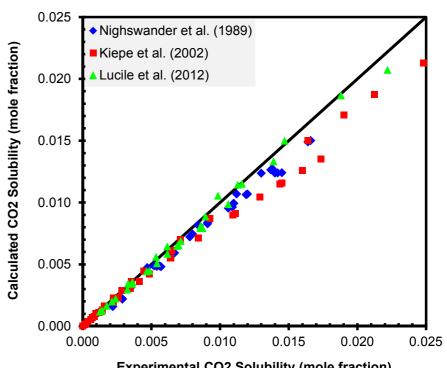


Solubility in Water



 Direct Henry's Constant Input

- Correlations
 - Harvey's Method
 - Li-Nghiem's Method
 - Account for Salinity





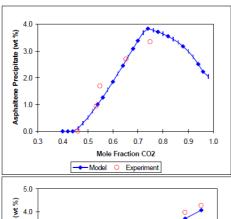


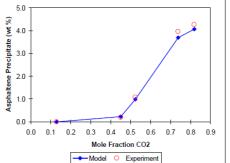
Asphaltene Precipitation

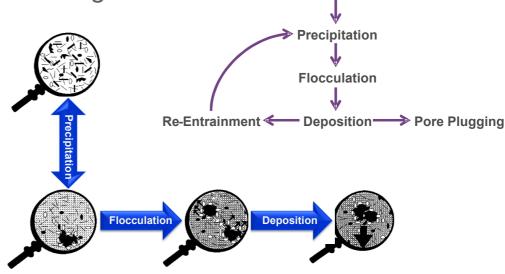


Change in *P*, *T*, or Composition

Asphaltene/Wax Modelling







Native Oil

Solvent (CO₂)



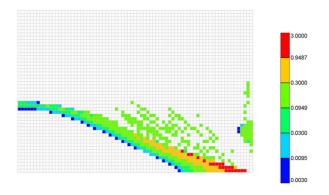


Flocculation and Deposition



Plugging and Permeability Impairment

- Flocculation
 - Aggregation into larger particles
 - Suspended component



- Deposition
 - Surface deposition, plugging deposition and re-entrainment
 - Non-equilibrium Blockage



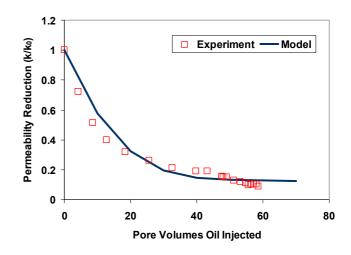


Blockage



- Resistance Factor Calculation
 - Power Law Model
 - Kozeny-Carman Equation
 - Solid Adsorption Model
- Permeability is divided by the resistance factor while calculating the phase transmissibilities

$$k = k_0 / rf$$

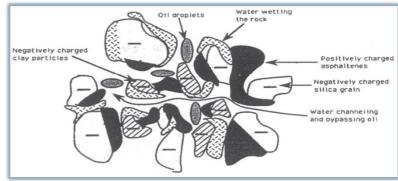




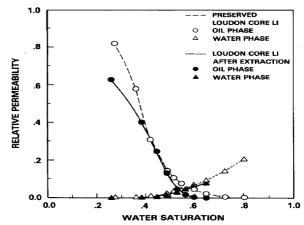
Wettability Alteration

GEM

- Wettability alteration
 - Asphaltene adsorption
 - Geochemical interaction/ion exchange
- Capillary pressure and relative permeability curves change
 - * KRINTRP
 - * INTCOMP



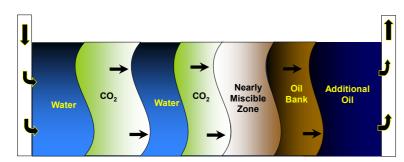
Leontaritis et al. 1994, SPE 23810.

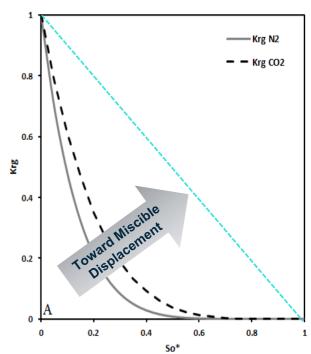






- Relative permeability as a function of IFT
- At higher IFT, typical relative permeability curves
- Straight line relative permeabilities as the IFT is lowered







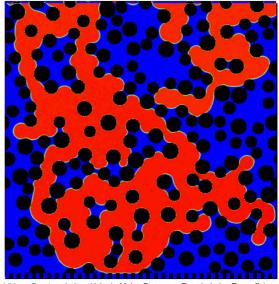


Hysteresis



A fluid (e.g. gas) moves into a pore:

- 1) Displaces fluid in pore (called drainage)
- 2) Sometimes displaced fluid moves back into the pore (called imbibition)
- 3) A shift in the Relative
 Permeability during this can trap
 some of the gas in the pore,
 making it immobile



Videos Courtesy Laboratório de Meios Porosos e Propriedades Termofísicas



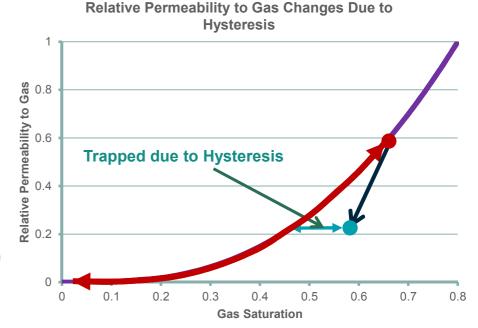


Hysteresis



A fluid (e.g. gas) moves into a pore

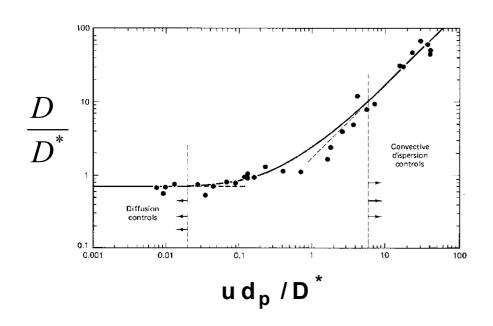
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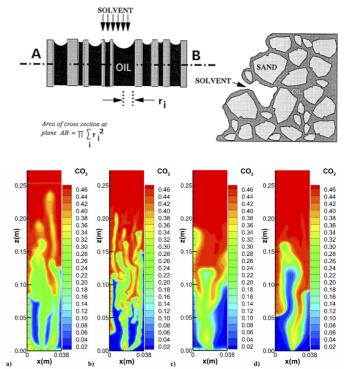




Diffusion and Dispersion









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Geomechanics

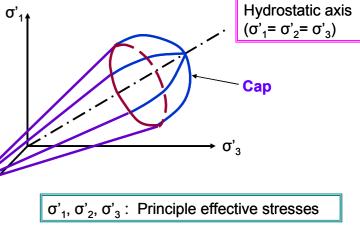


- Caprock integrity due to stress/strain relationships
- Different constitutive models
- Applications:

Risk assessment in sequestration

 Deformation of geological structure due to fluid withdrawal/injection

Geomechanical effects on coal-seams



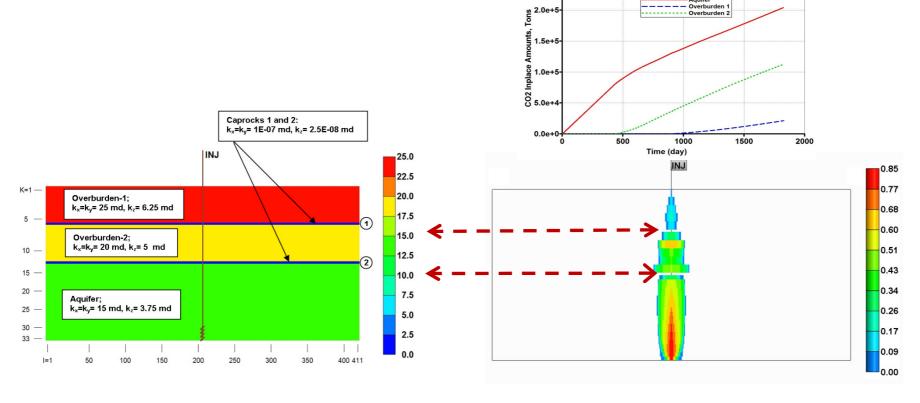
- ...





Geomechanics





2.5e+5-

--- Overburden 1 ----- Overburden 2

Advances in Hybrid EOR Processes

LSWI, Foam, etc.





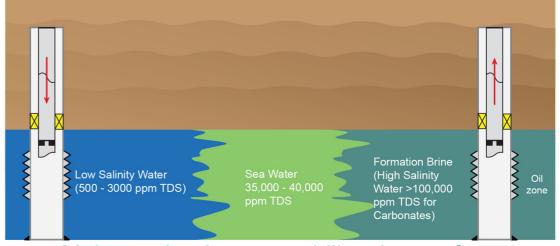
CO₂ + Low Salinity Water Flooding



LSW is attractive because:

- Operationally identical to conventional waterflooding
- No requirements for expensive chemicals
- Possible significant increase in recovery

LSW works in oil-wet reservoirs with clay



Main mechanism: wettability change from oil-wet to water-wet





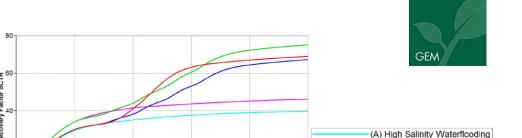
CO₂ WAG

- CO₂ Miscibility
- Mobility Control (WAG)
- High Recovery Factor
- Delayed Production Problem /



LSWI

- Wettability Alteration
- Higher Recovery w.r.t HSWI
- Lower Chemical Cost
- Environmental Impact
- Field Implementation
- Lower Recovery w.r.t Miscible Floods



800

1.000

CO₂ LSWAG

600

- Synergy of Mechanisms
- CO₂ Miscibility

200

- Mobility Control
- Wettability Alteration
- Geochemical Reaction with Inj CO₂
- Ion Exchange
- Dissolution of Carbonate Minerals
- Higher Recovery w.r.t HSWI, LSWI, CO₂ HSWAG, and pure CO₂
- No Challenge of late Production



(B) Low Salinity Waterflooding
(C) High Salinity WAG

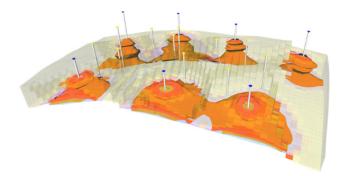
(D) Low Salinity WAG
(E) Pure CO2 Flooding

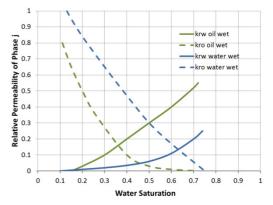


CO₂ LSWAG in GEM



- EOS compositional simulator
- Full geochemistry model
 - Aqueous reactionsE.g. CO2(aq) + H2O = (H+) + (HCO3-)
 - lon exchange equilibriaE.g. (Na+) + 0.5(Ca-X2) = 0.5(Ca++) + (Na-X)
 - Mineral dissolution/precipitation reactions
 E.g. Calcite + (H+) = (Ca++) + (HCO3-)
- Interpolation between oil-wet and water-wet relative permeability based on ion exchange
- Models temperature effects on low salinity









Foam Assisted CO₂ EOR

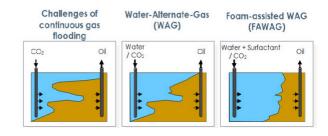


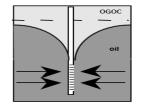
Gas Mobility Control

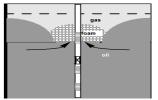
- Improve the sweep efficiency in bypassed oil zones
- Foam is used to change the mobility of gas in the reservoir

Gas Shut-Off

 Foam around perforations reduce gas mobility and production in wells located near the gas oil contact









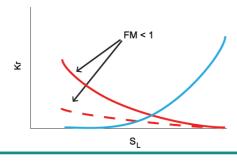


Advances in Foam Modelling



Modification of Relative Permeability

- Uses FM as interpolant
 - FM = 0 Strong Foam
 - FM = 1 No Foam
- Use FM as a multiplier to krg



Dependencies

- FMMOB: Foam Mobility
- F1: Surfactant Concentration
- F2: Oil Saturation
- F3 & F4: Capillary Number
- F5: Oil Composition
- F6: Salinity
- FDRY: Foam Dry Out

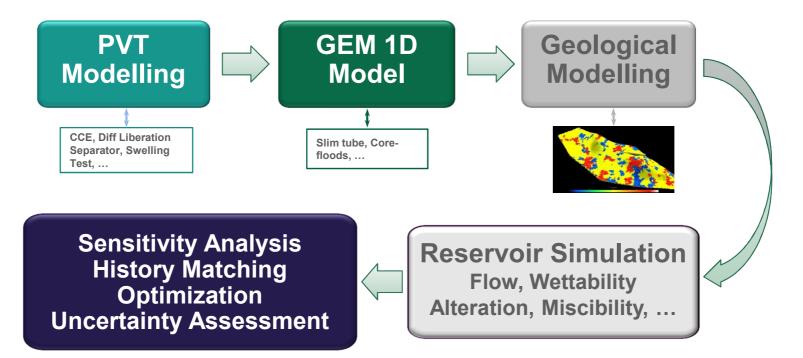
$$FM = \frac{1}{1 + FMMOB * F1 * F2 * F3 * F4 * F5 * F6 * FDRY}$$



Practical Workflow



Practical Work Flow





Case Studies





Case Studies

Case 1: Field-scale inverted 5-spot pattern model

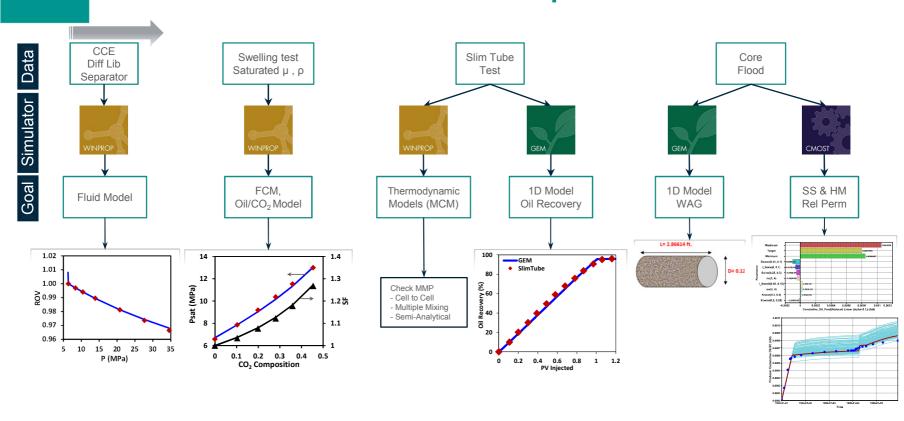
Application of workflow

Case 2: Field scale model

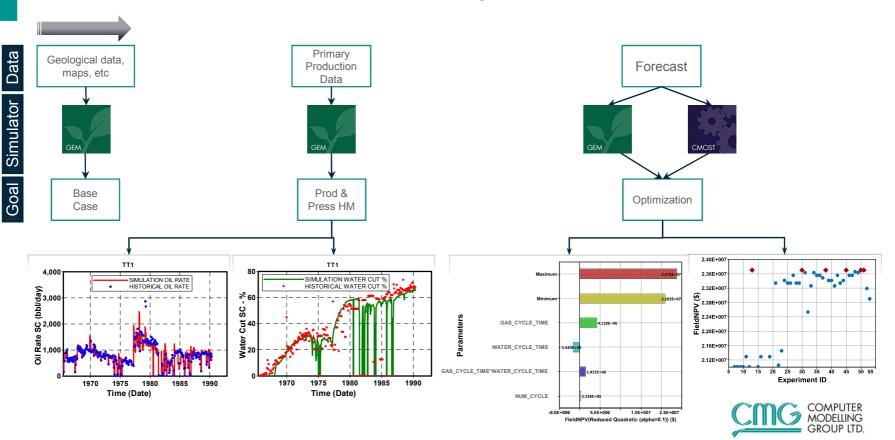
- Primary and Secondary Recovery HM
- WAG optimization
- Evaluation of Mechanisms



Case 1: Field-Scale 5-spot Model



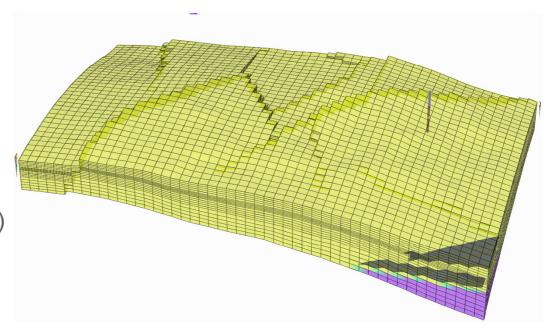
Case 1: Field-Scale 5-spot Model



Case 2: Field Scale Model

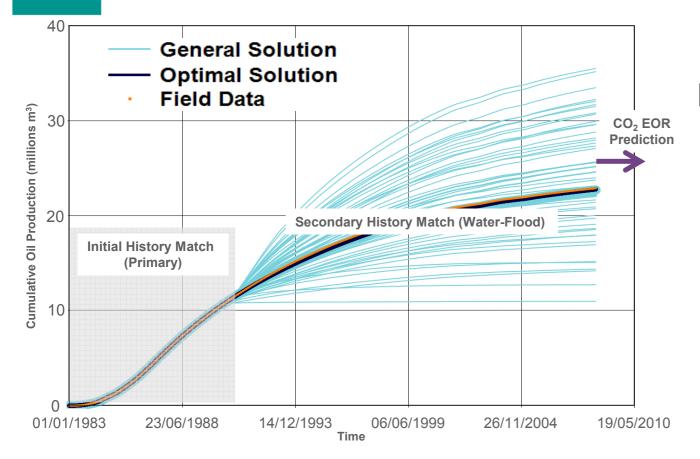
Original Oil in Place (OOIP): 684.6 million barrels

- Start with 7 years of primary production (1983-1990)
- Followed by 18 years of water-flooding (1990-2008)
- Water-flooding followed by CO₂ WAG process from 2008-2035





Case 2: Multiple-Stage History Match

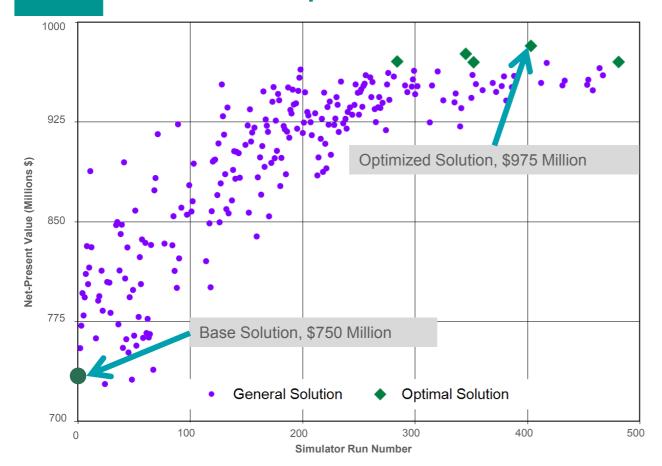


Needed to match

- Bottom-hole pressures
- Cumulative oil production
 - Per well
 - Entire field
- From 1983 2008



Case 2: Optimization of WAG Process



Optimized NPV

- Base NPV
 - \$750 Million
- Optimized NPV
 - \$975 Million
- Slug sizes
- Injection pressures
- Producer water-cut& GOR controls





Case 2: Physics Included

EOS phase behaviour

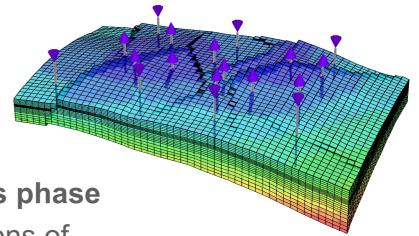
 Correctly accounts for phase changes of oil and CO₂

FCM and **MCM** determinations

Viscosity alteration

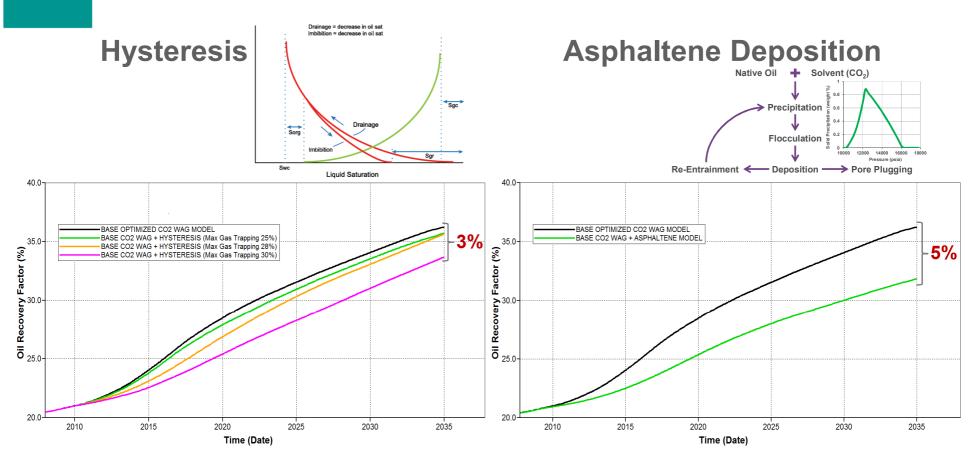
Solubility of CO₂ in the aqueous phase

Viscosity and density alterations of aqueous phase





Case 2: Additional Considerations



Capabilities for Carbon Management

GEM

Geochemical EOS compositional simulator for CO₂ storage in saline aquifers

Modelling of CO₂ solubility and brine properties

Solubility trapping

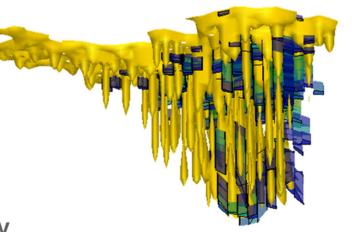
Relative permeability hysteresis

Residual gas trapping

Aqueous chemical equilibrium reactions and mineral dissolution and precipitation kinetics

- CO₂ mineralization

Geo-mechanics to model the cap rock integrity based on stress/strain relationships





Conclusions

- CMG accurately models CO₂ related processes and mechanisms
- PVT modelling and data matching (WinProp)
- GEM multiphase multicomponent EOS thermal flow simulator
 - CO₂ Flooding, WAG, Foam, Polymer, ASP, LSWI, ...
 - Low Salinity + Miscible + Foam + ASP
 - GEM is only commercial simulator that models combination of processes
- Full geochemistry model (aqueous reactions, ion-exchange, mineral dissolution, ...)
- Geomechanics Module
- Sensitivity study, history matching, optimization, uncertainty analysis (CMOST)
- No other simulator/package can do all of this!